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Supplementary material

SUPPLEMENTARY MATERIAL (ELECTRONIC VERSION ONLY) TO Derived thermodynamic properties of alcohol + cyclohexylamine mixtures

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Table I. Partial molar volumes, $\overline{V_i}$, partial excess molar volumes, $\overline{V_i}^{\rm E}$, thermal expansion coefficients, α , excess thermal expansion coefficients, $\alpha^{\rm E}$, and isothermal coefficients of pressure excess molar enthalpy, $(\partial H^{\rm E}/\partial P)_{T,x}$, for alcohol (1) + cyclohexylamine (2) binary mixtures at different temperatures (288.15 to 323.15) K and atmospheric pressure

		-			-	-	
x_1	α	α^{E}	$(\partial H^{\rm E}/\partial p)_{T,x}$	${}_{3}\overline{V_{1}}$	${}_{3}^{V_{2}}$	\bar{V}_{1}^{E}	V_{2}^{E}
	10 K	10 K	J-MPa -mol	cm ·mol	cm ·mol	cm ∙mol	cm ⋅mol
		1-P	ropanol (1) + cy	clohexylam	ine (2)		
			T = 288	3.15 K			
0.0000	1.041	0	0	70.303 ^b	113.827	-4.1012^{d}	0
0.0509	1.034	-5.77	0.0439	70.458	113.823	-3.9462	-0.0032
0.1017	1.029	-9.73	0.0265	70.610	113.811	-3.7939	-0.0160
0.1486	1.025	-11.89	-0.0338	70.784	113.786	-3.6201	-0.0411
0.1992	1.023	-12.85	-0.1351	71.006	113.739	-3.3985	-0.0880
0.3007	1.021	-11.51	-0.4031	71.541	113.558	-2.8633	-0.2691
0.4009	1.021	-7.78	-0.6734	72.148	113.227	-2.2563	-0.5999
0.4998	1.021	-3.75	-0.8650	72.766	112.718	-1.6382	-1.1090
0.6002	1.020	-1.48	-0.9235	73.350	112.002	-1.0543	-1.8250
0.7000	1.015	-1.7	-0.8197	73.830	111.108	-0.5740	-2.7183
0.7997	1.008	-3.89	-0.5725	74.170	110.093	-0.2345	-3.7336
0.8500	1.005	-4.95	-0.4137	74.282	109.566	-0.1224	-4.2603
0.8998	1.002	-5.23	-0.2526	74.355	109.059	-0.0496	-4.7673
0.9502	1.001	-3.91	-0.1054	74.394	108.585	-0.0107	-5.2419
1.0000	1.001	0	0	74.404	108.193 ^c	0	-5.6334 ^e
			T = 293	3.15 K			
0.0000	1.047	0	0	70.576	114.423	-4.1970	0
0.0509	1.040	-5.23	0.0288	70.757	114.419	-4.0168	-0.0038
0.1017	1.035	-8.73	-0.0011	70.929	114.405	-3.8447	-0.0182

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IADLL	I. Commuc	u								
<i>x</i> ₁	$\alpha_{10^{-3} \text{ K}^{-1}}$	α^{E} 10 ⁻⁶ K ⁻¹	$(\partial H^{\rm E}/\partial p)_{T,x}$ I·MPa ⁻¹ ·mol ⁻¹	\bar{V}_1	\bar{V}_2	$\bar{V}_1^{\rm E}$	$\overline{V}_2^{\rm E}$			
	10 11	10 II 1-P	ropanol(1) + cv	clohexvlam	nine (2)	chi hioi				
			T = 293	15 K						
0 1486	1.032	-10.53	0 0709	71 117	114 378	-3 6560	_0.0454			
0.1992	1.032	-11 17	-0.1803	71 352	114 328	-34218	-0.0950			
0.3007	1.029	-9.42	-0.4582	71 902	114 142	-2.8709	-0.2812			
0.3007	1.029	-5.51	-0.7315	72.515	113 808	-2.2579	-0.6151			
0.4998	1.029	-1.5	-0.9211	73.134	113.299	-1.6397	-1.1242			
0.6002	1.027	0.63	-0.9739	73.715	112.586	-1.0579	-1.8376			
0.7000	1.022	0.16	-0.8619	74.194	111.695	-0.5791	-2.7281			
0.7997	1.015	-2.4	-0.6041	74.534	110.678	-0.2390	-3.7456			
0.8500	1.011	-3.72	-0.4390	74.648	110.145	-0.1257	-4.2779			
0.8998	1.008	-4.32	-0.2708	74.722	109.628	-0.0515	-4.7950			
0.9502	1.006	-3.40	-0.1152	74.762	109.137	-0.0113	-5.2865			
1.0000	1.006	0	0	74.773	108.721	0	-5.7025			
	T = 298.15 K									
0.0000	1.052	0	0	70.295	115.026	-4.2873	0			
0.0509	1.046	-4.70	0.0135	71.066	115.021	-4.0826	-0.0044			
0.1017	1.041	-7.74	-0.0292	71.257	115.005	-3.8915	-0.0204			
0.1486	1.039	-9.19	-0.1086	71.460	114.976	-3.6887	-0.0496			
0.1992	1.037	-9.52	-0.2262	71.706	114.924	-3.4426	-0.1017			
0.3007	1.036	-7.35	-0.5142	72.272	114.733	-2.8769	-0.2926			
0.4009	1.036	-3.28	-0.7906	72.890	114.396	-2.2585	-0.6293			
		1-P	ropanol (1) + cy	clohexylar	nine (2)					
			T = 298	3.15 K						
0.4998	1.037	0.73	-0.9781	73.508	113.888	-1.6406	-1.1381			
0.6002	1.034	2.71	-1.0252	74.087	113.177	-1.0611	-1.8485			
0.7000	1.029	1.99	-0.9047	74.564	112.290	-0.5840	-2.7360			
0.7997	1.021	-0.94	-0.6362	74.905	111.270	-0.2434	-3.7555			
0.8500	1.017	-2.51	-0.4647	75.019	110.733	-0.1290	-4.2931			
0.8998	1.014	-3.42	-0.2893	75.095	110.206	-0.0534	-4.8201			
0.9502	1.011	-2.9	-0.1252	75.137	109.698	-0.0119	-5.3279			
1.0000	1.011	0	0	74.582	109.258	0	-5.7679			
			T = 308	3.15 K						
0.0000	1.063	0	0	71.468	116.248	-4.4513	0			
0.0509	1.058	-3.66	-0.0180	71.719	116.243	-4.2003	-0.0055			
0.1017	1.054	-5.81	-0.0869	71.945	116.224	-3.9735	-0.0244			
0.1486	1.052	-6.57	-0.1860	72.175	116.191	-3.7441	-0.0574			
0.1992	1.051	-6.29	-0.3203	72.443	116.134	-3.4760	-0.1141			
0.3007	1.051	-3.31	-0.6290	73.035	115.935	-2.8837	-0.3136			
0.4009	1.052	1.1	-0.9118	73.662	115.594	-2.2567	-0.6547			
0.4998	1.052	5.09	-1.0951	74.278	115.087	-1.6404	-1.1620			
0.6002	1.049	6.79	-1.1303	74.852	114.383	-1.0665	-1.8656			
0.7000	1.044	5.59	-0.9926	75.326	113.502	-0.5931	-2.7462			
() 7997	1 035	1 94	-0.7022	75 667	112 480	-0.2517	-3 7686			

TABLE I. Continued

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	α	$\alpha^{\rm E}$	$(\partial H^{\rm E}/\partial p)_{T,x}$	$\overline{V_1}$	\overline{V}_2	$\overline{V}_{1}^{\mathrm{E}}$	$\overline{V}_2^{\mathrm{E}}$		
x_1	10^{-3} K^{-1}	10^{-6} K^{-1}	J·MPa ⁻¹ ·mol ⁻¹	$cm^3 \cdot mol^{-1}$	$cm^3 \cdot mol^{-1}$	$cm^{3} \cdot mol^{-1}$	$cm^3 \cdot mol^{-1}$		
		1-Pı	ropanol $(1) + cy$	clohexylam	ine (2)				
			T = 308	.15 K					
0.8500	1.031	-0.12	-0.5175	75.784	111.932	-0.1353	-4.3163		
0.8998	1.026	-1.64	-0.3272	75.862	111.386	-0.0570	-4.8623		
0.9502	1.023	-1.91	-0.1456	75.906	110.847	-0.0131	-5.4016		
1.0000	1.022	0	0	75.919	110.361	0	-5.8876		
T = 313.15 K									
0.0000	1.069	0	0	71.790	116.869	-4.5251	0		
0.0509	1.064	-3.15	-0.0341	72.063	116.863	-4.2521	-0.0060		
0.1017	1.061	-4.86	-0.1164	72.307	116.843	-4.0086	-0.0263		
0.1486	1.059	-5.28	-0.2257	72.548	116.808	-3.7670	-0.0610		
0.1992	1.058	-4.7	-0.3685	72.826	116.749	-3.4887	-0.1198		
0.3007	1.058	-1.32	-0.6879	73.431	116.545	-2.8845	-0.3232		
0.4009	1.059	3.25	-0.9739	74.061	116.202	-2.2542	-0.6660		
0.4998	1.060	7.22	-1.1550	74.676	115.695	-1.6395	-1.1719		
0.6002	1.057	8.78	-1.1841	75.247	114.995	-1.0686	-1.8718		
0.7000	1.051	7.34	-1.0376	75.718	114.118	-0.5973	-2.7486		
0.7997	1.042	3.35	-0.7359	76.059	113.094	-0.2557	-3.7720		
0.8500	1.037	1.04	-0.5445	76.177	112.541	-0.1383	-4.3243		
0.8998	1.032	-0.79	-0.3466	76.256	111.986	-0.0588	-4.8793		
0.9502	1.029	-1.44	-0.1561	76.302	111.431	-0.0136	-5.4337		
1.0000	1.027	0	0	76.315	110.927	0	-5.9419		
		1-B	utanol $(1) + cyc$	lohexylami	ne $(2)^a$				
			T = 288	3.15 K					
0.0000	1.041	0	0	87.398	113.827	-3.7317	0		
0.0499	1.030	-6.75	0.0930	87.553	113.823	-3.5771	-0.0035		
0.1019	1.022	-10.8	0.0899	87.707	113.810	-3.4224	-0.0164		
0.1499	1.017	-12.31	0.0217	87.871	113.787	-3.2591	-0.0400		
0.1997	1.013	-12.25	-0.0930	88.064	113.745	-3.0652	-0.0814		
0.2995	1.007	-9.39	-0.3822	88.529	113.588	-2.6007	-0.2382		
0.4000	1.002	-5.25	-0.6546	89.076	113.291	-2.0534	-0.5354		
0.4994	0.996	-2.02	-0.8266	89.647	112.822	-1.4830	-1.0043		
0.6006	0.988	-0.59	-0.8621	90.193	112.152	-0.9366	-1.6744		
0.6977	0.978	-1.1	-0.7602	90.626	111.350	-0.5032	-2.4768		
0.7497	0.972	-1.63	-0.6585	90.807	110.879	-0.3231	-2.9480		
0.7984	0.966	-2.39	-0.5410	90.938	110.430	-0.1919	-3.3968		
0.8500	0.960	-2.76	-0.4008	91.037	109.968	-0.0931	-3.8585		
0.8993	0.954	-2.77	-0.2608	91.095	109.565	-0.0350	-4.2611		
0.9508	0.949	-1.74	-0.1193	91.123	109.218	-0.0063	-4.6085		
1.0000	0.945	0	0	91.130	109.003	0	-4.8234		
0.0000	1.047	0	T = 293	5.15 K	114 400	2.0405	0		
0.0000	1.047	0	0	87.715	114.423	-5.8425	0		
0.0499	1.037	-5.86	0.0666	8/.906	114.419	-5.0514	-0.0044		
0.1019	1.029	-9.33	0.0532	88.088	114.404	-3.4692	-0.0195		

TABLE I. Continued

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III

TADLE	1. Continue	u				_	
<i>x</i> ₁	α	α^{E}	$(\partial H^{E}/\partial p)_{T,x}$	$3\overline{V_1}$	\overline{V}_2	$\overline{V}_1^{\mathrm{E}}$	$\overline{V}_2^{\mathrm{E}}$
	10 K	10 K 1_R	$J \cdot W ra \cdot mol$	lohexylami	$re(2)^a$	ciii ·moi	
		1-D	$\frac{T-200}{T}$	$\frac{1510}{215}$ K	(<i>2</i>)		
0.1400	1.024	10.00	I = 29	00 270	114 279	2 2070	0.0457
0.1499	1.024	-10.99	-0.0132	00.270 88.476	114.370	-3.2070	-0.0437
0.1997	1.020	-11.04	-0.1233	00.470 00.057	114.333	-3.0809	-0.0897
0.2995	1.014	-0.31	-0.4034	00.934 80.504	114.172	-2.0034	-0.2307
0.4000	1.009	-4.49	-0.0723	00.073	113.074	-2.0333	-0.3493
0.4994	0.005	-1.08	-0.8500	90.073	112 730	0.0401	-1.0109
0.0000	0.995	0.02	-0.7925	90.017	112.739	-0.9401 -0.5073	-1.0845 -2.4858
0.0977	0.984	_0.10	-0.6871	91.050	111.957	-0.3073	-2.4858
0.7497	0.978	-0.49	-0.5630	01 362	111.405	-0.3207	-2.7580
0.7504	0.972	-1.40 -2.18	-0.5050	91.302	110 548	-0.1950	-3.8756
0.8993	0.959	_2.10	-0.2653	91 521	110.340	-0.0361	-4 2851
0.0775	0.954	_1.75	_0 1178	91 551	109 781	-0.0066	-4 6427
1 0000	0.950	0	0.1170	91 557	109.701	0.0000	-4 8702
1.0000	0.750	0	$\frac{0}{T-298}$	8 15 K	107.555	0	4.0702
0.0000	1.052	0	0	88 050	115 026	_3 9406	0
0.0000	1.032	_4 99	0.0397	88 271	115.020	-37196	-0.0051
0.1019	1.036	-8.27	0.0158	88 476	115.021	-3 5141	-0.0221
0 1499	1.030	-9.68	-0.0528	88 674	114 975	-3 3167	-0.0506
0 1997	1.026	-9.85	-0.1582	88 893	114 929	-3.0977	-0.0972
0.2995	1.019	-7.65	-0.4249	89.384	114.763	-2.6067	-0.2625
0.4000	1.014	-3.75	-0.6906	89.938	114.463	-2.0527	-0.5630
0.4994	1.008	-0.18	-0.8738	90.506	113.996	-1.4848	-1.0298
0.6006	1.000	1.8	-0.9251	91.048	113.331	-0.9427	-1.6947
0.6977	0.990	1.4	-0.8255	91.479	112.532	-0.5111	-2.4937
0.7497	0.983	0.62	-0.7161	91.660	112.060	-0.3306	-2.9661
0.7984	0.977	-0.6	-0.5854	91.792	111.607	-0.1983	-3.4190
0.8500	0.970	-1.63	-0.4272	91.893	111.136	-0.0975	-3.8898
0.8993	0.964	-2.3	-0.2698	91.953	110.719	-0.0374	-4.3065
0.9508	0.958	-1.78	-0.1162	91.983	110.350	-0.0070	-4.6759
1.0000	0.954	0	0	91.990	110.106	0	-4.9194
			T = 308	3.15 K			
0.0000	1.063	0	0	88.781	116.248	-4.0982	0
0.0499	1.056	-3.28	-0.0154	89.041	116.242	-3.8379	-0.0061
0.1019	1.049	-5.81	-0.0609	89.281	116.223	-3.5985	-0.0258
0.1499	1.044	-7.13	-0.1298	89.504	116.190	-3.3750	-0.0581
0.1997	1.039	-7.51	-0.2256	89.745	116.139	-3.1344	-0.1092
0.2995	1.032	-5.96	-0.4691	90.264	115.965	-2.6153	-0.2836
0.4000	1.026	-2.29	-0.7279	90.829	115.659	-2.0501	-0.5900
0.4994	1.020	1.62	-0.9227	91.397	115.192	-1.4822	-1.0565
0.6006	1.013	4.12	-0.9902	91.934	114.533	-0.9450	-1.7152
0.6977	1.002	3.84	-0.8930	92.361	113.742	-0.5177	-2.5065
0 7497	0 995	2.81	-0.7755	92 541	113 272	_0 3380	-2 9768

TABLE I. Continued

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	α	a ^E	$(\partial H^{\rm E}/\partial p)_{T,x}$	$\overline{V_1}$	\bar{V}_2	$\overline{V}_{1}^{\mathrm{E}}$	$\overline{V}_{2}^{\mathrm{E}}$		
<i>x</i> ₁	10^{-3} K^{-1}	10^{-6} K^{-1}	J·MPa ⁻¹ ·mol ⁻¹	cm ³ ·mol ⁻¹	cm ³ ·mol ⁻¹	cm ³ ·mol ⁻¹	cm ³ ·mol ⁻¹		
		1-B	Sutanol $(1) + cyc$	lohexylami	ne $(2)^a$				
			T = 308	3.15 K					
0.7984	0.988	1.14	-0.6313	92.674	112.817	-0.2052	-3.4312		
0.8500	0.981	-0.53	-0.4545	92.776	112.339	-0.1030	-3.9094		
0.8993	0.973	-1.85	-0.2790	92.838	111.907	-0.0407	-4.3418		
0.9508	0.967	-1.83	-0.1129	92.871	111.509	-0.0080	-4.7396		
1.0000	0.963	0	0	92.879	111.223	0	-5.0250		
<i>T</i> = 313.15 K									
0.0000	1.069	0	0	89.178	116.869	-4.1578	0		
0.0499	1.063	-2.44	-0.0437	89.448	116.863	-3.8879	-0.0063		
0.1019	1.056	-4.61	-0.1002	89.698	116.842	-3.6379	-0.0269		
0.1499	1.051	-5.87	-0.1693	89.931	116.809	-3.4044	-0.0606		
0.1997	1.046	-6.37	-0.2602	90.182	116.755	-3.1543	-0.1138		
0.2995	1.038	-5.13	-0.4918	90.715	116.576	-2.6206	-0.2930		
0.4000	1.032	-1.57	-0.7469	91.288	116.266	-2.0480	-0.6031		
0.4994	1.027	2.5	-0.9477	91.857	115.799	-1.4792	-1.0703		
0.6006	1.019	5.27	-1.0236	92.391	115.144	-0.9448	-1.7255		
0.6977	1.009	5.04	-0.9276	92.815	114.358	-0.5205	-2.5113		
0.7497	1.002	3.9	-0.8060	92.994	113.890	-0.3417	-2.9793		
0.7984	0.994	2	-0.6549	93.127	113.436	-0.2090	-3.4334		
0.8500	0.986	0	-0.4685	93.230	112.954	-0.1061	-3.9149		
0.8993	0.979	-1.63	-0.2837	93.293	112.514	-0.0426	-4.3556		
0.9508	0.972	-1.84	-0.1113	93.327	112.099	-0.0086	-4.7701		
1.0000	0.968	0	0	93.336	111.788	0	-5.0814		
		1-P	entanol $(1) + cy$	clohexylam	ine (2)				
			T = 288	3.15 K					
0.0000	1.041	0	0	104.434	113.827	-3.2902	0		
0.0506	1.027	-7.79	0.1404	104.539	113.824	-3.1855	-0.0025		
0.1001	1.015	-12.78	0.1912	104.644	113.815	-3.0809	-0.0111		
0.1500	1.006	-15.45	0.1704	104.772	113.797	-2.9528	-0.0296		
0.2002	0.998	-16.21	0.0921	104.929	113.763	-2.7959	-0.0631		
0.2997	0.987	-13.82	-0.1696	105.326	113.629	-2.3984	-0.1980		
0.3995	0.979	-8.61	-0.4705	105.819	113.361	-1.9054	-0.4659		
0.5004	0.970	-3.65	-0.7025	106.360	112.915	-1.3643	-0.9116		
0.6003	0.959	-1.1	-0.7812	106.870	112.289	-0.8543	-1.5380		
0.6998	0.944	-1.57	-0.6790	107.288	111.513	-0.4370	-2.3131		
0.7962	0.928	-3.99	-0.4365	107.562	110.705	-0.1631	-3.1216		
0.8500	0.919	-5.21	-0.2727	107.653	110.283	-0.0719	-3.5437		
0.8995	0.912	-5.44	-0.1321	107.701	109.952	-0.0239	-3.8751		
0.9501	0.906	-4.04	-0.0280	107.721	109.707	-0.0034	-4.1196		
1.0000	0.903	0	0	107.725	109.578	0	-4.2484		
			T = 293	3.15 K					
0.0000	1.047	0	0	104.799	114.423	-3.4079	0		
0.0506	1.033	-7.03	0.1185	104.936	114.420	-3.2708	-0.0033		

TABLE I. Continued

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TADLL	TABLE I. Continued								
<i>x</i> ₁	$\alpha_{10^{-3} K^{-1}}$	$\alpha^{\rm E}$ 10 ⁻⁶ K ⁻¹	$(\partial H^{E}/\partial p)_{T,x}$	\bar{V}_1	\bar{V}_2	$\overline{V}_1^{\mathrm{E}}$	$V_2^{\rm E}$		
	10 K	10 K 1-P	$\frac{J \cdot WFa}{Ventanol(1) + cv}$	clohexylam	$\frac{1}{1}$				
			$\frac{T-202}{T-202}$						
0.1001	1.022	116	0 1575	105.067	114 400	2 1 4 0 1	0.0140		
0.1001	1.022	-11.0	0.1373	105.007	114.409	-3.1401	-0.0140		
0.1300	1.015	-14.09	0.1522	105.210	114.300	-2.9911	-0.0333		
0.2002	1.003	-14.60	0.0330	105.369	114.551	-2.0101	-0.0724		
0.2997	0.994	-12.82	-0.1940	105.800	114.210	-2.4011	-0.2130		
0.3995	0.985	-8.14	-0.4799	106.305	113.938	-1.9016	-0.4849		
0.5004	0.975	-3.55	-0.7012	106.845	113.494	-1.3019	-0.9292		
0.6003	0.964	-1.05	-0.7792	107.351	112.8/3	-0.8562	-1.5502		
0.6998	0.949	-1.26	-0.6855	107.765	112.104	-0.4423	-2.3192		
0.7962	0.934	-3.31	-0.4550	108.039	111.296	-0.1685	-3.1276		
0.8500	0.925	-4.39	-0.2957	108.131	110.867	-0.0760	-3.5559		
0.8995	0.917	-4.64	-0.1551	108.181	110.524	-0.0264	-3.8994		
0.9501	0.911	-3.48	-0.0442	108.203	110.258	-0.0042	-4.1650		
1.0000	0.907	0	0	108.207	110.097	0	-4.3266		
	T = 298.15 K								
0.0000	1.052	0	0	105.180	115.026	-3.5162	0		
0.0506	1.039	-6.29	0.0962	105.346	115.022	-3.3503	-0.0040		
0.1001	1.028	-10.44	0.1231	105.500	115.009	-3.1964	-0.0166		
0.1500	1.019	-12.75	0.0933	105.668	114.985	-3.0284	-0.0408		
0.2002	1.012	-13.52	0.0172	105.856	114.945	-2.8405	-0.0809		
0.2997	1.000	-11.85	-0.2200	106.291	114.798	-2.4052	-0.2280		
0.3995	0.990	-7.68	-0.4895	106.797	114.523	-1.8990	-0.5026		
0.5004	0.980	-3.46	-0.7000	107.336	114.079	-1.3600	-0.9463		
0.6003	0.968	-1.01	-0.7772	107.838	113.463	-0.8579	-1.5629		
0.6998	0.954	-0.96	-0.6922	108.249	112.699	-0.4468	-2.3266		
0.7962	0.938	-2.63	-0.4738	108.523	111.891	-0.1732	-3.1349		
0.8500	0.930	-3.58	-0.3190	108.617	111.457	-0.0796	-3.5685		
0.8995	0.922	-3.85	-0.1785	108.668	111.103	-0.0285	-3.9225		
0.9501	0.916	-2.92	-0.0608	108.691	110.819	-0.0048	-4.2066		
1.0000	0.911	0	0	108.696	110.629	0	-4.3972		
			T = 308	3.15 K					
0.0000	1.063	0	0	105.994	116.248	-3.7048	0		
0.0506	1.051	-4.84	0.0506	106.207	116.243	-3.4920	-0.0052		
0.1001	1.041	-8.16	0.0527	106.399	116.228	-3.2998	-0.0209		
0.1500	1.032	-10.11	0.0135	106.599	116.199	-3.0997	-0.0496		
0.2002	1.025	-10.9	-0.0602	106.812	116.153	-2.8861	-0.0951		
0.2997	1.012	-9.94	-0.2722	107.281	115.995	-2.4178	-0.2530		
0.3995	1.001	-6.77	-0.5091	107.801	115.714	-1.8978	-0.5348		
0.5004	0.990	-3.27	-0.6975	108.341	115.269	-1.3578	-0.9790		
0.6003	0.978	-0.93	-0.7730	108.838	114.659	-0.8604	-1.5896		
0.6998	0.964	-0.36	-0.7059	109.245	113.903	-0.4538	-2.3453		
0.7962	0.948	-1.3	-0.5123	109.518	113.096	-0.1806	-3.1530		
0.8500	0.940	_1 99	_0.3669	109 613	112 654	_0.0853	_3 5946		

TABLE I. Continued

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	α	$\alpha^{\rm E}$	$(\partial H^{\rm E}/\partial p)_{T\rm r}$	$\overline{V_1}$	\overline{V}_2	$\overline{V_1}^{\mathrm{E}}$	$\overline{V}_{2}^{\mathrm{E}}$			
x_1	10^{-3} K^{-1}	10^{-6} K^{-1}	J·MPa ⁻¹ ·mol ⁻¹	$cm^3 \cdot mol^{-1}$	$cm^3 \cdot mol^{-1}$	$cm^{3} \cdot mol^{-1}$	$cm^{3} \cdot mol^{-1}$			
		1-P	entanol $(1) + cy$	clohexylam	ine (2)					
			T = 308	3.15 K						
0.8995	0.932	-2.28	-0.2264	109.667	112.284	-0.0319	-3.9649			
0.9501	0.925	-1.82	-0.0948	109.693	111.970	-0.0059	-4.2781			
1.0000	0.919	0	0	109.699	111.733	0	-4.5155			
	<i>T</i> = 313.15 K									
0.0000	1.069	0	0	106.427	116.869	-3.7850	0			
0.0506	1.058	-4.13	0.0272	106.657	116.864	-3.5543	-0.0056			
0.1001	1.048	-7.04	0.0166	106.865	116.847	-3.3469	-0.0226			
0.1500	1.039	-8.82	-0.0274	107.078	116.816	-3.1338	-0.0532			
0.2002	1.032	-9.61	-0.0999	107.302	116.768	-2.9094	-0.1010			
0.2997	1.018	-9	-0.2990	107.785	116.606	-2.4263	-0.2637			
0.3995	1.006	-6.32	-0.5191	108.313	116.320	-1.8992	-0.5491			
0.5004	0.995	-3.19	-0.6962	108.854	115.875	-1.3575	-0.9946			
0.6003	0.983	-0.88	-0.7708	109.350	115.265	-0.8613	-1.6038			
0.6998	0.969	-0.07	-0.7129	109.756	114.513	-0.4561	-2.3567			
0.7962	0.954	-0.65	-0.5320	110.029	113.705	-0.1832	-3.1638			
0.8500	0.945	-1.21	-0.3914	110.124	113.261	-0.0873	-3.6081			
0.8995	0.937	-1.51	-0.2509	110.179	112.885	-0.0331	-3.9842			
0.9501	0.929	-1.29	-0.1122	110.205	112.561	-0.0063	-4.3081			
1.0000	0.923	0	0	110.212	112.306	0	-4.5631			
		2-В	Sutanol $(1) + cyc$	clohexylam	ine (2)					
			T = 288	3.15 K						
0.0000	1.041	0	0	88.673	113.827	-2.7586	0			
0.0495	1.039	-2.31	-0.0177	88.773	113.823	-2.6582	-0.0034			
0.1011	1.037	-3.88	-0.0625	88.921	113.811	-2.5102	-0.0156			
0.1505	1.036	-4.6	-0.1253	89.076	113.789	-2.3551	-0.0380			
0.1995	1.036	-4.68	-0.2013	89.244	113.753	-2.18/1	-0.0738			
0.3004	1.037	-3.34	-0.3765	89.631	113.622	-1.8003	-0.2042			
0.3996	1.039	-1.12	-0.5335	90.046	113.398	-1.3858	-0.4290			
0.49/4	1.041	0.77	-0.6323	90.454	113.064	-0.9778	-0.7622			
0.5997	1.042	1.8	-0.6446	90.838	112.597	-0.5937	-1.2298			
0.7000	1.041	1.25	-0.5546	91.134	112.04/	-0.2972	-1.7794			
0./999	1.039	-0.37	-0.3789	91.327	111.4/4	-0.1048	-2.3522			
0.8488	1.038	-1.19	-0.2745	91.382	111.210	-0.0493	-2.0100			
0.8997	1.038	-1.03	-0.1632	91.415	110.987	-0.0101	-2.8400			
0.9498	1.038	-1.38	-0.0692	91.429	110.823	-0.0024	-3.0037			
1.0000	1.039	U	$\frac{0}{T-202}$	91.431 8 15 K	110./18	0	-3.1001			
0.0000	1.047	0	$\frac{1-293}{0}$	80 087	114 423	_2 8071	0			
0.0000	1.047	_2 67	_0 0045	89.002	114.420	-2.0071 -2.6957	_0.0037			
0.1011	1.047	_4 55	_0.00+5	89 352	114 407	_2.573	-0.0037			
0.1505	1.041	-5 52	_0.0902	89 515	114 383	_2.3373	_0.0403			
0.1995	1.041	-5.84	-0.1609	89.690	114.346	-2.1999	-0.0774			

TABLE I. Continued

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VII

TABLE	TABLE I. Conunued								
<i>x</i> ₁	$\frac{\alpha}{10^{-3} \text{ K}^{-1}}$	10^{-6} K^{-1}	$(\partial H^{\rm E}/\partial p)_{T,x}$ J·MPa ⁻¹ ·mol ⁻¹	$cm^{3} \cdot mol^{-1}$	$\overline{V_2}$ cm ³ ·mol ⁻¹	$\overline{V}_1^{\rm E}$ cm ³ ·mol ⁻¹	$\overline{V}_2^{\mathrm{E}}$ cm ³ ·mol ⁻¹		
		2-F	$\frac{1}{3}$ utanol (1) + cyc	lohexylam	ine (2)				
			$\frac{T-203}{T-203}$	8 15 K					
0.3004	1.041	_1 97	1 = 275	90.08/	11/ 213	_1 8052	_0.2104		
0.3004	1.041	_3.29	-0.5221	90.004	113 087	-1.3052 -1.3878	-0.2104		
0.3770	1.043	_1.97	_0 5481	90.902	113.507	_0 9799	_0.7698		
0.4274	1.044	_1.57	_0 5452	91 293	113 187	-0 5968	-1 2361		
0.7000	1.043	-2.48	-0.4462	91 589	112 639	-0.3010	-1 7846		
0.7999	1.041	_4	-0.2756	91 782	112.063	-0.1078	-2 3598		
0.8488	1.040	-4 46	-0.1823	91.838	111 801	-0.0517	-2.6220		
0.8997	1.040	-4.23	-0.0928	91.872	111.565	-0.0174	-2.8584		
0.9498	1.041	-2.91	-0.0267	91.887	111.391	-0.0028	-3.0327		
1.0000	1.044	0	0	91.890	111.269	0	-3.1539		
			T = 298	3.15 K					
0.0000	1.052	0	0	89.500	115.026	-2.8609	0		
0.0495	1.049	-3.02	0.0090	89.624	115.022	-2.7375	-0.0040		
0.1011	1.047	-5.21	-0.0136	89.793	115.008	-2.5678	-0.0179		
0.1505	1.045	-6.43	-0.0589	89.965	114.983	-2.3961	-0.0427		
0.1995	1.045	-6.98	-0.1199	90.146	114.945	-2.2155	-0.0812		
0.3004	1.045	-6.59	-0.2667	90.548	114.809	-1.8128	-0.2168		
0.3996	1.046	-5.42	-0.3946	90.969	114.581	-1.3926	-0.4445		
0.4974	1.046	-4.68	-0.4624	91.376	114.248	-0.9847	-0.7775		
0.5997	1.046	-4.83	-0.4441	91.759	113.783	-0.6026	-1.2427		
0.7000	1.044	-6.16	-0.3359	92.054	113.234	-0.3067	-1.7913		
0.7999	1.042	-7.58	-0.1706	92.249	112.654	-0.1121	-2.3713		
0.8488	1.042	-7.69	-0.0886	92.306	112.386	-0.0547	-2.6394		
0.8997	1.043	-6.78	-0.0192	92.342	112.140	-0.0190	-2.8855		
0.9498	1.045	-4.43	0.0166	92.358	111.952	-0.0033	-3.0742		
1.0000	1.049	0	0	92.361	111.809	0	-3.2167		
			T = 308	3.15 K					
0.0000	1.063	0	0	90.366	116.248	-2.9837	0		
0.0495	1.059	-3.72	0.0367	90.516	116.244	-2.8332	-0.0048		
0.1011	1.056	-6.51	0.0370	90.711	116.228	-2.6389	-0.0207		
0.1505	1.054	-8.22	0.0097	90.901	116.200	-2.4489	-0.0481		
0.1995	1.053	-9.22	-0.0356	91.095	116.159	-2.2546	-0.0894		
0.3004	1.052	-9.74	-0.1530	91.514	115.018	-1.8357	-0.2302		
0.3990	1.052	-9.57	-0.2509	91.939	115./88	-1.4105	-0.4605		
0.4974	1.052	-9.95	-0.2807	92.347	113.433	-1.0030	-0.7931		
0.3997	1.030	-11.24 12.22	-0.2307	72.120 03.025	114.991	0.0219	1 8080		
0.7000	1.046	-13.32	-0.1098	95.025	112.842	-0.5244	-1.6069		
0.1999	1.040	_13.08	0.0440	93.225	113.042	-0.1243	-2.4003 -2.6021		
0.0400	1.047	-13.90	0.1030	93.200	113.330	-0.0032	-2.0921		
0.0797	1.049	_7 39	0.1054	93 345	113.262	-0.0233	-2.2000		
1.0000	1.060	0	0	93.350	112.855	0	-3.3935		

TABLE I. Continued

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	α	α ^E	$(\partial H^{\rm E}/\partial p)_{T,x}$	$\overline{V_1}$	\overline{V}_2	\overline{V}_{1}^{E}	$\overline{V}_2^{\mathrm{E}}$		
<i>x</i> ₁	10^{-3} K^{-1}	10^{-6} K^{-1}	J·MPa ⁻¹ ·mol ⁻¹	$cm^3 \cdot mol^{-1}$	$cm^3 \cdot mol^{-1}$	$cm^3 \cdot mol^{-1}$	$cm^3 \cdot mol^{-1}$		
		2-E	Butanol (1) + cyc	clohexylami	ine (2)				
			T = 313	3.15 K					
0.0000	1.069	0	0	90.817	116.869	-3.0529	0		
0.0495	1.065	-4.06	0.0508	90.982	116.864	-2.8873	-0.0052		
0.1011	1.062	-7.14	0.0629	91.190	116.847	-2.6795	-0.0221		
0.1505	1.060	-9.09	0.0449	91.390	116.818	-2.4797	-0.0510		
0.1995	1.058	-10.31	0.0075	91.591	116.775	-2.2782	-0.0938		
0.3004	1.057	-11.27	-0.0948	92.019	116.632	-1.8510	-0.2372		
0.3996	1.056	-11.58	-0.1773	92.446	116.400	-1.4235	-0.4687		
0.4974	1.055	-12.5	-0.1966	92.853	116.068	-1.0163	-0.8011		
0.5997	1.053	-14.35	-0.1304	93.234	115.604	-0.6355	-1.2648		
0.7000	1.050	-16.8	0.0061	93.533	115.049	-0.3364	-1.8199		
0.7999	1.049	-17.94	0.1551	93.737	114.439	-0.1322	-2.4298		
0.8488	1.050	-17.04	0.2023	93.801	114.142	-0.0686	-2.7274		
0.8997	1.052	-14.2	0.2092	93.843	113.850	-0.0264	-3.0194		
0.9498	1.057	-8.83	0.1508	93.864	113.596	-0.0055	-3.2728		
1.0000	1.066	0	0	93.870	113.362	0	-3.5075		
2-Methyl-2-propanol (1) + cyclohexylamine (2)									
			T = 308	3.15 K					
0.0000	1.063	0	0	92.833	116.248	-3.4054	0		
0.0508	1.068	-8.5	0.1874	92.939	116.244	-3.3006	-0.0050		
0.1002	1.074	-16.19	0.3500	93.142	116.227	-3.0978	-0.0217		
0.1502	1.081	-23.51	0.5020	93.364	116.195	-2.8758	-0.0536		
0.2001	1.088	-30.53	0.6477	93.596	116.145	-2.6437	-0.1030		
0.3005	1.105	-43.97	0.9423	94.074	115.985	-2.1654	-0.2637		
0.3991	1.122	-56.84	1.2505	94.534	115.736	-1.7051	-0.5123		
0.4996	1.141	-69.35	1.5772	94.974	115.377	-1.2659	-0.8719		
0.5998	1.164	-79.42	1.8698	95.368	114.893	-0.8714	-1.3551		
0.6997	1.194	-84.09	2.0368	95.708	114.261	-0.5320	-1.9872		
0.7999	1.235	-78.08	1.9322	95.981	113.437	-0.2585	-2.8114		
0.8712	1.277	-62.86	1.5790	96.125	112.704	-0.1149	-3.5445		
0.8992	1.296	-53.77	1.3533	96.167	112.376	-0.0724	-3.8723		
0.9504	1.339	-30.83	0.7831	96.221	111.710	-0.0185	-4.5385		
1.0000	1.389	0	0	96.239	111.019	0	-5.2294		
0.0000	1.0.00		T = 313	<u>3.15 K</u>	116060	2 5202			
0.0000	1.069	0	0	93.386	116.869	-3.5203	0		
0.0508	1.075	-/.99	0.1727	93.499	116.864	-5.4088	-0.0052		
0.1002	1.082	-15.39	0.3290	93.708	116.84/	-5.1991	-0.0225		
0.1502	1.089	-22.61	0.4814	93.936	116.814	-2.9/17	-0.0551		
0.2001	1.096	-29.68	0.6325	94.172	116.764	-2.7355	-0.1054		
0.3005	1.112	-43.48	0.9463	94.656	116.601	-2.2512	-0.2681		
0.3991	1.129	-56.7	1.2/2/	95.122	116.349	-1./854	-0.5197		
0.4996	1.149	-09.25	1.6055	95.569	115.983	-1.5581	-0.8860		
0.3998	1.1/3	-/8./8	1.8853	95.976	115.485	-0.9314	-1.3844		

TABLE I. Continued

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INDEL	1. Continued	1					
<i>x</i> ₁	10^{-3} K^{-1}	10^{-6} K^{-1}	$(\partial H^{\mathrm{E}}/\partial p)_{T,x}$ J·MPa ⁻¹ ·mol ⁻¹	$cm^{3} \cdot mol^{-1}$	$cm^{3} \cdot mol^{-1}$	$\overline{V}_{1}^{\mathrm{E}}$ cm ³ ·mol ⁻¹	$\overline{V}_2^{\mathrm{E}}$ cm ³ ·mol ⁻¹
		2-Methy	1-2-propanol (1)	+ cyclohex	xylamine (2)	
			T = 313	3.15 K	2	,	
0.6997	1.204	-82.44	2.0224	96.332	114.822	-0.5757	-2.0474
0.7999	1.247	-75.4	1.8839	96.624	113.940	-0.2834	-2.9293
0.8712	1.289	-59.98	1.5188	96.780	113.142	-0.1270	-3.7275
0.8992	1.309	-51.07	1.2948	96.827	112.781	-0.0804	-4.0879
0.9504	1.350	-29.01	0.7420	96.887	112.043	-0.0207	-4.8261
1.0000	1.399	0	0	96.907	111.266	0	-5.6027
		-	T = 318	3.15 K		-	
0.0000	1.075	0	0	93.966	117.497	-3.6291	0
0.0508	1.081	-7.48	0.1578	94.082	117.492	-3.5137	-0.0054
0.1002	1.088	-14.6	0.3077	94.297	117.474	-3.2992	-0.0230
0.1502	1.095	-21.72	0.4604	94.528	117.441	-3.0681	-0.0562
0.2001	1.103	-28.85	0.6170	94.767	117.390	-2.8290	-0.1071
0.3005	1.119	-43	0.9504	95.256	117.225	-2.3395	-0.2715
0.3991	1.137	-56.57	1.2953	95.729	116.970	-1.8674	-0.5266
0.4996	1.157	-69.12	1.6343	96.186	116.596	-1.4105	-0.9009
0.5998	1.182	-78.13	1.9011	96.606	116.081	-0.9903	-1.4161
0.6997	1.214	-80.78	2.0078	96.979	115.386	-0.6175	-2.1114
0.7999	1.259	-72.74	1.8349	97.290	114.447	-0.3065	-3.0501
0.8712	1.301	-57.12	1.4576	97.458	113.587	-0.1382	-3.9098
0.8992	1.321	-48.39	1.2353	97.508	113.196	-0.0876	-4.3005
0.9504	1.362	-27.22	0.7002	97.573	112.393	-0.0226	-5.1044
1.0000	1.409	0	0	97.595	111.539	0	-5.9579
			T = 323	3.15 K			
0.0000	1.081	0	0	94.572	118.130	-3.7317	0
0.0508	1.087	-6.98	0.1426	94.689	118.125	-3.6153	-0.0054
0.1002	1.095	-13.83	0.2861	94.906	118.107	-3.3982	-0.0233
0.1502	1.103	-20.85	0.4391	95.139	118.074	-3.1651	-0.0568
0.2001	1.110	-28.02	0.6013	95.380	118.022	-2.9242	-0.1081
0.3005	1.127	-42.52	0.9545	95.874	117.856	-2.4302	-0.2740
0.3991	1.144	-56.42	1.3182	96.353	117.597	-1.9511	-0.5329
0.4996	1.165	-68.99	1.6636	96.821	117.214	-1.4832	-0.9164
0.5998	1.191	-77.47	1.9171	97.256	116.680	-1.0479	-1.4502
0.6997	1.225	-79.14	1.9930	97.647	115.951	-0.6573	-2.1791
0.7999	1.271	-70.12	1.7851	97.976	114.957	-0.3280	-3.1736
0.8712	1.314	-54.31	1.3955	98.156	114.039	-0.1483	-4.0915
0.8992	1.333	-45.77	1.1749	98.210	113.620	-0.0941	-4.5100
0.9504	1.374	-25.46	0.6578	98.280	112.757	-0.0243	-5.3735
1.0000	1.419	0	0	98.304	111.835	0	-6.2949

TABLE I. Continued

^aCalculations for system 1-butanol + cyclohexylamine are based on literature experimental data³; ^bpartial molar volume at infinite dilution $\overline{V_1^{\infty}}$ at $x_1 = 0$; ^cpartial molar volume at infinite dilution $\overline{V_2^{\infty}}$ at $x_1 = 1$; ^dpartial excess molar volume at infinite dilution $\overline{V_2^{\infty}}$ at $x_1 = 1$; ^dpartial excess molar volume at infinite dilution $\overline{V_2^{\infty}}$ at $x_1 = 1$

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T/V	V_1°	V_2°	$\overline{V_1}^{\infty}$	$\overline{V_2}^{\infty}$	$\overline{V}_{1}^{\mathrm{E},\infty}$	$\overline{V}_{2}^{\mathrm{E},\infty}$
1 / K	cm ³ ·mol ⁻¹	$cm^3 \cdot mol^{-1}$	cm ³ ·mol ⁻¹	$cm^{3} \cdot mol^{-1}$	cm ³ ·mol ⁻¹	cm ³⁻ mol ⁻¹
		1-Propanol	(1) + cycloh	exylamine (2)		
288.15	74.404	113.827	70.388	107.992	-4.0167	-5.8346
293.15	74.773	114.423	70.662	108.534	-4.1111	-5.8894
298.15	75.148	115.026	70.946	109.083	-4.2023	-5.9428
303.15	75.530	115.634	71.241	109.638	-4.2896	-5.9959
308.15	75.919	116.248	71.555	110.206	-4.3637	-6.0421
313.15	76.315	116.869	71.886	110.800	-4.4289	-6.0689
		1-Butanol	(1) + cyclohe	exylamine (2)		
288.15	91.130	113.827	87.493	108.706	-3.6363	-5.1205
293.15	91.557	114.423	87.820	109.244	-3.7373	-5.1794
298.15	91.990	115.026	88.166	109.811	-3.8246	-5.2152
303.15	92.431	115.634	88.519	110.380	-3.9118	-5.2538
308.15	92.879	116.248	88.890	110.959	-3.9889	-5.2896
313.15	93.336	116.869	89.281	111.544	-4.0544	-5.3251
		1-Pentanol	(1) + cycloh	exylamine (2)		
288.15	107.7247	113.827	104.588	109.374	-3.1369	-4.4529
293.15	108.2070	114.423	104.961	109.918	-3.2460	-4.5056
298.15	108.6963	115.026	105.338	110.466	-3.3586	-4.5601
303.15	109.1931	115.634	105.730	111.024	-3.4627	-4.6106
308.15	109.6986	116.248	106.145	111.589	-3.5537	-4.6595
313.15	110.2117	116.869	106.576	112.182	-3.6354	-4.6873
		2-Butanol	(1) + cyclohe	exylamine (2)		
288.15	91.431	113.827	88.651	110.572	-2.7800	-3.2544
293.15	91.890	114.423	89.067	111.125	-2.8223	-3.2985
298.15	92.361	115.026	89.471	111.672	-2.8903	-3.3541
303.15	92.847	115.634	89.889	112.209	-2.9587	-3.4249
308.15	93.350	116.248	90.327	112.736	-3.0222	-3.5120
313.15	93.870	116.869	90.786	113.252	-3.0831	-3.6169
	2-	Methyl-2-prop	anol(1) + cy	yclohexylamin	e (2)	
303.15	95.591	115.634	92.137	110.729	-3.4535	-4.9046
308.15	96.239	116.248	92.663	110.969	-3.5752	-5.2791
313.15	96.907	116.869	93.215	111.220	-3.6922	-5.6494
318.15	97.595	117.497	93.790	111.494	-3.8057	-6.0032
323.15	98.304	118.130	94.395	111.795	-3.9089	-6.3352

TABLE II. Molar volumes, V_1° and V_2° , partial molar volumes at infinite dilution, $\overline{V_1}^{\infty}$ and $\overline{V_2}^{\infty}$, and partial excess molar volumes at infinite dilution, $\overline{V_1}^{E,\infty}$ and $\overline{V_2}^{E,\infty}$

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